# Dissociation of the anions $AIF_6^{3-}$ in the system Na<sub>3</sub>AIF<sub>6</sub>—Na<sub>2</sub>SO<sub>4</sub>

## I. KOŠTENSKÁ and M. MALINOVSKÝ

Department of Inorganic Technology, Slovak Technical University, 880 37 Bratislava

#### Received 31 May 1977

#### Accepted for publication 12 September 1977

## Dedicated to Professor Ing Dr Jaroslav Malkovský on his 75th birthday

The course of the liquidus of Na<sub>2</sub>SO<sub>4</sub> in the system Na<sub>3</sub>AlF<sub>6</sub>—Na<sub>2</sub>SO<sub>4</sub> was determined. The eutectic point was found to be at 9.0 mole % Na<sub>3</sub>AlF<sub>6</sub> and 91.0 mole % Na<sub>2</sub>SO<sub>4</sub>,  $t_E = 794.5^{\circ}$ C. The solubility of Na<sub>3</sub>AlF<sub>6</sub> in solid Na<sub>2</sub>SO<sub>4</sub> is negligible. The course of the liquidus curve of Na<sub>2</sub>SO<sub>4</sub> in the composition interval of 91.0—96.0 mole % Na<sub>2</sub>SO<sub>4</sub> is consistent with the assumption that the anions AlF<sub>6</sub><sup>-</sup> undergo thermal dissociation according to the scheme AlF<sub>6</sub><sup>-</sup>  $\Rightarrow$  AlF<sub>4</sub><sup>-</sup> + 2F<sup>-</sup>. At a very low content of Na<sub>3</sub>AlF<sub>6</sub> in Na<sub>2</sub>SO<sub>4</sub> a total destruction of the anions AlF<sub>4</sub><sup>-</sup> takes place under the formation of 7 new elementary particles from each molecule of Na<sub>3</sub>AlF<sub>6</sub> in molten Na<sub>2</sub>SO<sub>4</sub>. In the eutectic point of the system Na<sub>3</sub>AlF<sub>6</sub>—Na<sub>2</sub>SO<sub>4</sub> the degree of thermal dissociation of AlF<sub>6</sub><sup>--</sup> anions according to the given scheme equals 0.67. The calculated dissociation degree of pure cryolite is 0.21. The conclusions of some other papers concerning the given problems are discussed.

Измерен ход ликвидуса Na<sub>2</sub>SO<sub>4</sub> в системе Na<sub>3</sub>AlF<sub>6</sub>—Na<sub>2</sub>SO<sub>4</sub>. Обнаружена эвтектическая точка при 9,0 мол. % Na<sub>3</sub>AlF<sub>6</sub> и 91,0 мол. % Na<sub>2</sub>SO<sub>4</sub>,  $t_{\rm E}$ =794,5°C. Растворимость Na<sub>3</sub>AlF<sub>6</sub> в твердом Na<sub>2</sub>SO<sub>4</sub> пренебрежимо мала. Ход кривых ликвидуса Na<sub>2</sub>SO<sub>4</sub> в интервале состава 91,0—96,0 мол. % Na<sub>2</sub>SO<sub>4</sub> консистентный в соответствии с предпосылкой того, что анионы AlF<sub>6</sub><sup>3-</sup> диссоциируют термически по схеме AlF<sub>6</sub><sup>3-</sup>  $\Rightarrow$  AlF<sub>4</sub><sup>-</sup> + 2F<sup>-</sup>. При очень низком содержании Na<sub>3</sub>AlF<sub>6</sub> в Na<sub>2</sub>SO<sub>4</sub> происходит также полное разложение анионов AlF<sub>4</sub><sup>-</sup>, причем из одной молекулы Na<sub>3</sub>AlF<sub>6</sub> образуется в расплаве Na<sub>2</sub>SO<sub>4</sub> 7 новых элементарных частиц. В эвтектической точке системы Na<sub>3</sub>AlF<sub>6</sub>—Na<sub>2</sub>SO<sub>4</sub> степень термической диссоциации анионов AlF<sub>6</sub><sup>3-</sup> по указанной схеме равна 0,67. Рассчитанная степень термической диссоциации чистого криолита равна 0,21. Обсуждаются заключения некоторых работ, посвященных этой тематике.

As indicated by numerous papers [1-11], the thermal dissociation of cryolite in the liquid state is a topical problem in the research of fused salts. Several authors

applied to their study the classical thermodynamic approach, described *e.g.* by *Glasstone* [12]. Its principle lies in comparing the experimentally established course of the liquidus of Na<sub>3</sub>AlF<sub>6</sub> in the system Na<sub>3</sub>AlF<sub>6</sub>—MA with the course calculated under certain simplifying assumptions. In this case, however, the system Na<sub>3</sub>AlF<sub>6</sub>—MA has to fulfil several conditions [1, 2, 4, 5]. In 1959 *Grjotheim et al.* [13] suggested for the determination of the character of thermal dissociation of Na<sub>3</sub>AlF<sub>6</sub> not to analyze liquidus curve of Na<sub>3</sub>AlF<sub>6</sub>, but that of the component MA in the system Na<sub>3</sub>AlF<sub>6</sub>—MA (the method of "the second component"). As the component MA sodium sulfate was chosen. This forms with cryolite a system with a eutectic. In the composition interval with a high content of Na<sub>3</sub>AlF<sub>6</sub> there is a wide region of solid solutions, while the Na<sub>3</sub>AlF<sub>6</sub> is practically insoluble in solid Na<sub>2</sub>SO<sub>4</sub> just as it is required if applying the method of "the second component". The data published by *Grjotheim et al.* [13] were confirmed in [14].

The degree of thermal dissociation of cryolite in equilibrium

$$Na_3AIF_6 \rightleftharpoons NaAIF_4 + 2NaF$$
 (A)

should be designated as d; apparently it holds that  $d = f_1(x_1) = f_2(x_2)$ ;  $x_1$  and  $x_2$  are mole fractions of Na<sub>3</sub>AlF<sub>6</sub> and Na<sub>2</sub>SO<sub>4</sub>, respectively;  $(x_1 + x_2 = 1)$ . If the temperature interval is not too wide  $(T_2^t - T_2 \le 100^{\circ}\text{C})$ , for the equilibrium activity of the component MA in its saturated solution,  $a_{2,eq}^t$ , the known relation is valid

$$\ln a_{2,eq}^{I} = (\Delta H_{2}^{f}/R)(1/T_{2}^{f} - 1/T_{2})$$
(1)

where  $\Delta H_2^t$  is the molar melting enthalpy of the pure component MA,  $T_2^t$  is the melting temperature [K] of the pure component MA, and  $T_2$  is the temperature [K] of the liquidus of component MA in the liquid phase, when its equilibrium activity is equal to  $a_{2,eq}^t$ .

The activity  $a_{2,eq}^{1}$  is a function of the parameter *d*. We choose different schemes of thermal dissociation and under the assumption of an ideal behaviour of the mixture Na<sub>3</sub>AlF<sub>6</sub> + MA, we may express the quantity  $a_{2,eq}^{1}$ . If a proper scheme was chosen, then the slope of the linear dependence log  $a_{2,eq}^{1} = f(1/T_{2}^{t} - 1/T_{2})$  is equal  $\Delta H_{2}^{t}/R$ . Since the systems NaCl—Na<sub>2</sub>SO<sub>4</sub>, NaBr—Na<sub>2</sub>SO<sub>4</sub>, and Na<sub>2</sub>CO<sub>3</sub>—Na<sub>2</sub>SO<sub>4</sub> are nearly ideal, *Grjotheim et al.* [13] suggest that also the mixture of the ions Na<sup>+</sup>, F<sup>-</sup>, AlF<sup>3</sup><sub>4</sub>, AlF<sup>3-</sup><sub>6</sub>, and SO<sup>2-</sup><sub>4</sub> (*i.e.* the molten binary system Na<sub>3</sub>AlF<sub>6</sub>—Na<sub>2</sub>SO<sub>4</sub>) will exhibit an ideal behaviour, thus justifying the application of Temkin's model of ideal ionic solutions [15].

In [13] it was stated, however, that for all the three chosen schemes

$$Na_{3}AlF_{6} \rightleftharpoons 2NaF + NaAlF_{4} \rightarrow 3Na^{+} + 2F^{-} + AlF_{4}^{-}$$
(B)

$$Na_{3}AlF_{6} \rightleftharpoons 3NaF + AlF_{3} \rightarrow 3Na^{+} + Al^{3+} + 6F^{-}$$
(C)

 $Na_3AlF_6 \rightleftharpoons 3Na^+ + AlF_6^{3-}$  (D)

the dependence  $a_{2,eq}^{!} = f(1/T)$  had the form of a curve, convex with respect to the axis of reciprocal temperature coordinates. According to *Grjotheim et al.* [13] this fact was due to a nonideal behaviour of the given system and they therefore suggested that  $\Delta \bar{H}_{Na_2SO_4,mix}^{!} \neq 0$ . In order to eliminate the effect of this quantity they drew tangents to the curves  $a_{2,eq}^{!} = f(1/T)$  for  $x_2 \rightarrow 1$  and from the slopes of these tangents they calculated the value of the parameter  $\Delta H_2^{!}$ .

For the first of the above schemes, *i.e.* (*B*), the obtained value conforms very good with the calorimetric data. Thus it may be expected that at a low content of cryolite in the given system the anions  $F^-$ ,  $AIF_4^-$ , and  $SO_4^{2-}$  are present in the melt.

The method used in [13] may be exactly justified. For a not too wide temperature interval  $(T_2^f - T_2)$  the simplified form of the general Le Chatelier—Shreder equation is valid [1]. If we consider the formation of a liquid solution from pure liquid substances "1" and "2", it holds

$$\Delta \bar{G}_{2,\text{mix}}^{1} = \Delta \bar{H}_{2,\text{mix}}^{1} - T \,\Delta \bar{S}_{2,\text{mix}}^{1} \tag{2}$$

According to the definition, it holds

$$\Delta \bar{G}_{2,\text{mix}}^{1} = \bar{G}_{2}^{1} - G_{2}^{0,1} = RT \ln a_{2}^{1}$$
(3)

For the case of formation of a liquid solution which is in equilibrium with solid substance "2", the activities in eqns (1) and (3) are equal and it holds

$$\ln a_{2,eq}^{l} = (\Delta \bar{H}_{2,mix}^{l}/RT_{2})_{eq} - (\Delta \bar{S}_{2,mix}^{l}/R)_{eq} = (\Delta H_{2}^{f}/R)(1/T_{2}^{f} - 1/T_{2})$$
(4)

For a system with the behaviour of Temkin's ideal solution  $\Delta \bar{H}_{2,\text{mix}}^{1}=0$  and therefore

$$\ln a_{2,\text{eq.Tem}}^{l} = -(\Delta \bar{S}_{2,\text{mix}}^{l}/R)_{\text{eq}} = (\Delta H_{2}^{f}/R)(1/T_{2}^{f} - 1/T_{2})$$
(5)

The term  $a_{2,eq,Tem}^{1}$  stands for the equilibrium activity of substance "2" in the liquid solution expressed according to Temkin. In a number of cases the behaviour of real solutions differs from the one postulated by Temkin's model. Then it holds

 $\ln a_{2,eq}^{\perp} \neq \ln a_{2,eq,Tem}^{\perp}$ 

This deviation from an ideal behaviour according to Temkin's model can be expressed quantitatively as the partial molar enthalpy of mixing of Na<sub>2</sub>SO<sub>4</sub>,  $\Delta \bar{H}^{1}_{2,\text{mix}}$ , however, it must be assumed that the value of the partial molar excess entropy of mixing of Na<sub>2</sub>SO<sub>4</sub>,  $\Delta \bar{S}^{\text{ex.l}}_{2,\text{mix}}$ , is negligible. Then it holds

$$\ln a_{2,eq}^{l} = \ln a_{2,eq,Tem}^{l} + (\Delta H_{2,mix}^{l}/RT_{2})_{eq}$$
(6)

and with respect to eqn (4)

$$\ln a_{2,\text{eq,Tem}}^{l} = (\Delta H_{2}^{f}/R)(1/T_{2}^{f}-1/T_{2}) - (\Delta \bar{H}_{2,\text{mix}}^{l}/RT_{2})_{\text{eq}}$$
(7)

Chem. zvesti 32 (6) 821-829 (1978)

823

For  $x_2 \rightarrow 1$ ,  $\Delta \bar{H}_{2,\text{mix}}^1 \rightarrow 0$  and consequently  $a_{2,\text{eq.Tem}}^1 \rightarrow a_{2,\text{eq.}}^1$ 

In order to approximate the experimental values to the straight line with the slope  $\Delta H_2^t/R$ , *Grjotheim et al.* [13] suggested that in the molten mixture Na<sub>3</sub>AlF<sub>6</sub>—Na<sub>2</sub>SO<sub>4</sub> the thermal dissociation of the AlF<sub>6</sub><sup>3-</sup> anions according to the scheme AlF<sub>6</sub><sup>3-</sup>  $\rightleftharpoons$  AlF<sub>4</sub><sup>-</sup> + 2F<sup>-</sup> took place. The degree of this dissociation is assumed to be dependent on cryolite content in the melt.

Let  $x_1$  and  $x_2$  be the mole fractions of Na<sub>3</sub>AlF<sub>6</sub> and Na<sub>2</sub>SO<sub>4</sub>, respectively. If the degree of thermal dissociation of Na<sub>3</sub>AlF<sub>6</sub> into NaAlF<sub>4</sub> and 2NaF is designated as d, then in the equilibrium mixture there exist

| $x_1(1-d)$    | moles of $AlF_6^{3-}$     |
|---------------|---------------------------|
| $x_1d$        | moles of AlF <sub>4</sub> |
| $2x_1d$       | moles of F-               |
| $3x_1 + 2x_2$ | moles of Na <sup>+</sup>  |

The equilibrium constant of thermal dissociation according to the scheme  $AlF_6^{3-} \rightleftharpoons AlF_4^- + 2F^-$  in the given mixture can be expressed as follows

$$K_{\rm dis} = \frac{4x_1^2 d^3}{(1-d)(1+2x_1 d)^2} \tag{8}$$

When deriving the relation (8) it was assumed that the considered molten mixture behaved like Temkin's ideal solution. Further it has been assumed that the constant of the thermal dissociation  $K_{dis}$  is temperature independent. This assumption can be satisfactorily fulfilled when the analyzed liquidus curve does not cover a too wide temperature interval. In the given case this interval corresponds to the difference  $(T_{Na_2SO_4}^i - T_E) < 100^{\circ}C$  and therefore it can be expected that the postulate  $K_{dis} \neq f(T)$  does not introduce any greater inaccuracy into the results. The degree of thermal dissociation, d, is supposed to be unambiguously defined by eqn (8).

According to Temkin, for the activity of Na<sub>2</sub>SO<sub>4</sub> the equation holds

$$a_{2,eq,Tem}^{1} = x_{Na^{+}}^{2} x_{SO_{4}^{2}} = \frac{x_{2}}{1 + 2(1 - x_{2})d}$$
(9)

The value of  $K_{dis}$  determined by *Grjotheim* [1] equals 0.06 (at the melting temperature of cryolite 1010°C). Then for a given  $x_1$  we can determine the value of d from eqn (8), that of  $a_{2,eq,Tem}^{1}$  from eqn (9) and we can draw the dependence  $\ln a_{2,eq,Tem}^{1} = f(1/T)$ . Though the points obtained in this way are situated nearer to the straight line with the "correct" slope, the deviation, *e.g.* for the eutectic point is still considerable. Therefore in [13] also the value  $K_{dis} = 0.02$  has been used in order to approximate the points still more to the straight line. Nevertheless, the points fit to the straight line with the slope  $\Delta H_2^t/R$  only then, if  $K_{dis} = 0.013$ , this value being clearly different from  $K_{dis} = 0.06$  [1], or  $K_{dis} = 0.037$  [2].

The results presented in [13] support the dissociation scheme  $AlF_6^{3-} \rightarrow AlF_4^- + 2F^-$ , with d = 50-70%. The values obtained yield, however, a lower

equilibrium dissociation constant than those found by other methods. The considered system does not behave apparently like Temkin's ideal solution at a higher content of cryolite in  $Na_2SO_4$  and therefore the efforts to "approximate" the experimental points to the theoretical curve by choosing a low value of the dissociation constant is questionable.

Further, in [13] the authors did not consider the possibility of a total destruction of the anions  $AlF_6^{3-}$  at a low content of cryolite in the melt; such destruction has been found for  $x_{Na_3AlF_6} \rightarrow 0$  in the system  $Na_3AlF_6$ —BaCl<sub>2</sub> [16] and also in the system  $Na_3AlF_6$ —NaCl [17] by means of the cryometric method.

#### Experimental

The system Na<sub>3</sub>AlF<sub>6</sub>—Na<sub>2</sub>SO<sub>4</sub> was investigated using TA method in the composition range 0—12 mole % Na<sub>3</sub>AlF<sub>6</sub>. Fifteen mixtures from the region of the primary crystallization of Na<sub>2</sub>SO<sub>4</sub> and three from that of Na<sub>3</sub>AlF<sub>6</sub> were measured. Some of the experimental data are listed in Table 1. The parameters of the eutectic point are 9 mole % Na<sub>3</sub>AlF<sub>6</sub> and 91 mole % Na<sub>2</sub>SO<sub>4</sub>, the temperature of the eutectic crystallization being 794.5 ± 0.5°C. The fact that the temperature of eutectic crystallization has been recorded on the cooling curves also at low contents of Na<sub>3</sub>AlF<sub>6</sub> (Table 1) indicates that cryolite is practically insoluble in solid Na<sub>2</sub>SO<sub>4</sub>. It is well known that the classical thermodynamic approach can be applied to the

#### Table 1

System Na<sub>3</sub>AlF<sub>6</sub>—Na<sub>2</sub>SO<sub>4</sub> Experimental data on TPC and  $T_E$ 

| Na <sub>3</sub> AlF <sub>6</sub> | Na <sub>2</sub> SO <sub>4</sub> | TPC     | $T_{\rm E}$ |
|----------------------------------|---------------------------------|---------|-------------|
| mole %                           | mole %                          | °C      | °C          |
| 0.00                             | 100.00                          | 884.8   |             |
| 0.10                             | 99.90                           | 881.5   | 796.0       |
| 0.25                             | 99.75                           | 877.0   | _           |
| 0.50                             | 99.50                           | 872.0   | _           |
| 0.75                             | 99.25                           | 869.0   | 789.0       |
| 1.00                             | 99.00                           | 866.0   | 795.0       |
| 2.00                             | 98.00                           | 852.0   | 794.0       |
| 3.00                             | 97.00                           | 842.0   | 796.0       |
| 4.00                             | 96.00                           | 832.5   | 795.0       |
| 5.00                             | 95.00                           | . 823.0 | 794.0       |
| 6.00                             | 94.00                           | 815.0   | 794.5       |
| 7.00                             | 93.00                           | 808.0   | 795.0       |
| 8.00                             | 92.00                           | 800.0   | 794.5       |
| 9.00                             | 91.00                           | —       | 794.0       |
|                                  |                                 |         |             |

TPC — temperature of primary crystallization.

determination of the character of thermal dissociation of the substance MB on the basis of the course of the liquidus curve of the substance MA only when the substance MB is insoluble in the solid MA. This condition is apparently fulfilled in the given case.

## **Results and discussion**

Because the difference  $T_2^{t} - T_E = 884.8^{\circ}\text{C} - 794.5^{\circ}\text{C} = 90.3^{\circ}\text{C}$  is less than 100°C, it is possible to neglect the dependence of the enthalpy of melting of Na<sub>2</sub>SO<sub>4</sub> on temperature. For calculation of  $a_{2,eq}^{l}$  eqn (1) can be used; it holds

$$\Delta H_2^{\rm f} = 23.72 \text{ kJ mol}^{-1} = 5.67 \text{ kcal mol}^{-1}$$
 [18]

The cryometric treatment of experimental results shows that for  $x_2 \rightarrow 1$  it holds that  $k_{1/2} \rightarrow 7$ . The correction factor decreases rapidly with increasing content of cryolite in Na<sub>2</sub>SO<sub>4</sub> and it reaches the value of 2.2 at the eutectic composition. In the case of a total decomposition according to the scheme AlF<sub>6</sub><sup>3-</sup> $\rightarrow$ Al<sup>3+</sup> + 6F<sup>-</sup>,  $k_{1/2} = 7$ . If the complete decomposition AlF<sub>6</sub><sup>3-</sup> $\rightarrow$ AlF<sub>4</sub><sup>-</sup> + 2F<sup>-</sup> takes place, then  $k_{1/2} = 3$ . Consequently, the existence of the equilibrium

$$AIF_6^{3-} \rightleftharpoons AIF_4^- + 2F^-$$

requires that  $k_{1/2} < 3$ . Therefore it was necessary to calculate the values of the correction factors in dependence on composition. To this purpose the "universal" relationship

#### Table 2

Numerical values of the activity of Na<sub>2</sub>SO<sub>4</sub> in the molten Na<sub>3</sub>AlF<sub>6</sub>—Na<sub>2</sub>SO<sub>4</sub> mixtures calculated on the basis of eqn (1) and the values of the correction factor  $k_{1/2}$  computed using eqn (10)

| Mole fraction of Na <sub>2</sub> SO <sub>4</sub><br>$x_2$ | $-(1/T_2^t - 1/T_2) \cdot 10^5$ | Activity of Na <sub>2</sub> SO <sub>4</sub><br>$a_{2,eq}^{l}$ | Correction factor $k_{1/2}$ |
|---|---------------------------------|---|-----------------------------|
| 1.0000  | 0.0000                          | 1.0000  | 7.0                         |
| 0.9990  | 0.2468                          | 0.9930  | 6.9                         |
| 0.9975  | 0.5856                          | 0.9832  | 6.6                         |
| 0.9950  | 0.9653                          | 0.9728  | 5.5                         |
| 0.9925  | 1.1946                          | 0.9665  | 4.4                         |
| 0.9900  | 1.4252                          | 0.9600  | 4.0                         |
| 0.9800  | 2.5175                          | 0.9308  | 3.5                         |
| 0.9700  | 3.3145                          | 0.9098  | 3.1                         |
| 0.9600  | 4.0850                          | 0.8900  | 2.9                         |
| 0.9500  | 4.8688                          | 0.8704  | 2.7                         |
| 0.9400  | 5.5395                          | 0.8539  | 2.6                         |
| 0.9300  | 6.1346                          | 0.8394  | 2.4                         |
| 0.9200  | 6.8241                          | 0.8230  | 2.3                         |
| 0.9100  | 7.3035                          | 0.8119  | 2.2                         |

$$\ln a_{2,eq}^{1} = k_{1/2} \ln x_{2} \tag{10}$$

has been used. Here  $k_{1/2}$  denotes a parameter numerically equal to the number of elementary particles (entities), which arise in the system formed by pure substance "2" (*i.e.* by pure Na<sub>2</sub>SO<sub>4</sub>) when introducing 1 molecule of substance "1" (*i.e.* Na<sub>3</sub>AlF<sub>6</sub>) [19]. The results of calculations according to eqns (1) and (10) are presented in Table 2. With respect to the value of  $k_{1/2}$  there exist two regions in the composition interval 0—9 mole % Na<sub>3</sub>AlF<sub>6</sub>:

a) 0—3.5 mole % Na<sub>3</sub>AlF<sub>6</sub>, where it holds  $k_{1/2} \ge 3$ ; in this region a total decomposition of AlF<sub>6</sub><sup>3-</sup> anions and a partial decomposition of AlF<sub>4</sub><sup>-</sup> anions evidently takes place. For  $x_1 \rightarrow 0$  also the latter decomposition is complete and thus  $k_{1/2} = k_{1/2}^{s_1} = 7$ . It is clear that as far as  $k_{1/2} \ge 3$ , eqns (8) and (9) cannot be applied to this case.

b) 3.5—9 mole % Na<sub>3</sub>AlF<sub>6</sub>, where it holds  $k_{1/2} < 3$ ; in this composition region the equilibrium AlF<sub>6</sub><sup>3-</sup>  $\Rightarrow$  AlF<sub>4</sub><sup>-</sup> + 2F<sup>-</sup> can be suggested. In Fig. 1 the measured values of the liquidus temperature of Na<sub>2</sub>SO<sub>4</sub> in coordinates log  $x_2 = f(1/T_2^t - 1/T_2)$  are presented as well as the tangents to the liquidus curve of Na<sub>2</sub>SO<sub>4</sub> for  $x_2 \rightarrow 1$ , for alternatively 1 to 7 new (foreign) particles arising from 1 molecule of Na<sub>3</sub>AlF<sub>6</sub>.

It is evident that the conclusions which follow from the data presented in Fig. 1 hold the better the lower is the content of cryolite in the melt.

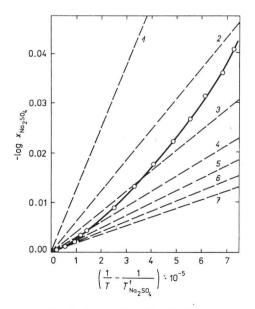


Fig. 1. System Na<sub>3</sub>AlF<sub>6</sub>—Na<sub>2</sub>SO<sub>4</sub>.

Experimental values of liquidus temperature of Na<sub>2</sub>SO<sub>4</sub> in the coordinates  $(1/T - 1/T'_{Na_2SO_4})$  vs. log  $x_{Na_2SO_4}$ .

$$k = 1; 2, k = 2; 3, k = 3; 4, k = 4; 5, k = 5; 6, k = 6; 7, k = 7$$

Chem. zvesti 32 (6) 821-829 (1978)

827

The above-mentioned relations enable to determine the degree d of thermal dissociation of  $AlF_6^{3-}$  anions. From eqn (9) it follows

$$d = \frac{x_2 - a_{2,eq,Tem}^1}{2(1 - x_2) a_{2,eq,Tem}^1}$$
(11)

Using eqn (1) we find  $a_{2,eq,E}^1 = 0.8119$ . For Temkin's ideal solution  $a_{2,eq,E}^1 = a_{2,eq,E,Tem}^1$ ; from eqn (11) it follows that d = 0.67. The parameters  $x_2 = 0.91$  and d = 0.67 inserted into eqn (8) yield the value  $K_{dis} = 0.024$ , which corresponds to the value of the thermal dissociation of pure cryolite, b = 0.21. Even though these data do not differ appreciably from the values of  $K_{dis} = 0.037$  and b = 0.25 reported in [2], it is evident that the melts of the system Na<sub>3</sub>AlF<sub>6</sub>—Na<sub>2</sub>SO<sub>4</sub> do not behave quite ideally, as postulated by Temkin's model. Their deviation from the Temkin ideal ionic solution can be expressed quantitatively as the magnitude of the partial molar enthalpy of mixing of Na<sub>2</sub>SO<sub>4</sub> in the given solution. For the sake of simplicity we shall suggest (as it has been done above) that the value of the excess partial entropy of mixing of Na<sub>2</sub>SO<sub>4</sub> is negligible.

We have mentioned already that  $a_{2,eq,E}^{1} = 0.8119$ . The most probable value of the degree of the thermal dissociation of pure cryolite is 0.25 [2, 10], which corresponds to the dissociation constant  $K_{dis} = 0.037$ . This value together with the value of  $x_{1,E} = 0.09$  inserted into eqn (8) yields  $d_{E} = 0.73$ . Then from eqn (9) we can calculate that  $a_{2,eq,E,Tem}^{1} = 0.8043$ .

From eqn (6) it follows

$$\Delta \bar{H}_{2,\text{mix,E}}^{1} = RT \ln \left( a_{2,\text{eq,E}}^{1} / a_{2,\text{eq,E,Tem}}^{1} \right) = 81.76 \text{ J mol}^{-1}$$
(12)

Suggesting that the system behaves like a strictly regular solution it holds

$$\Delta \bar{H}_{2,\text{mix,E}}^{1} = \omega (1 - x_{2,E})^{2}$$

from which  $\omega = 10.094 \text{ J mol}^{-1}$  can be determined. For the solution with the composition  $x_2 = 0.5$  the partial molar enthalpy of mixing of Na<sub>2</sub>SO<sub>4</sub> would reach

Table 3

| Comparison of the main | parameters of therma | l dissociation of | cryolite in the s | system Na <sub>3</sub> AlF <sub>6</sub> —Na <sub>2</sub> SO <sub>4</sub> |
|------------------------|----------------------|-------------------|-------------------|--|
|                        |                      |                   |                   |  |

| Ref. $a_{2.eq.E}^{1}$ |                        | $d_{E}$                                       |              | According to Temkin |      |
|-----------------------|------------------------|---|--------------|---------------------|------|
|                       | According<br>to Temkin | According to<br>the universal<br>relationship | $K_{ m dis}$ | b .                 |      |
| [13]                  | 0.8215                 | 0.58  | 0.53         | 0.013               | 0.17 |
| This paper            | 0.8119                 | 0.67  | 0.60         | 0.024               | 0.21 |

the value of 2523.5 J mol<sup>-1</sup>. Consequently, Na<sub>2</sub>SO<sub>4</sub> exhibits a weak positive deviation from an ideal ionic behaviour in this solution.

For the processing of the experimental results also the universal relationship [19] has been used. For the eutectic point E in the system  $Na_3AlF_6$ — $Na_2SO_4$  it holds

$$\ln a_{2,eq,E}^{I} = k_{1/2} \ln x_{2,E} \tag{13}$$

As  $a_{2,eq,E}^{!}=0.8119$  and  $x_{2,E}=0.91$ ,  $k_{1/2}=2.2$ . From the equation of the thermal dissociation of cryolite

$$x_1(1-d)$$
 Na<sub>3</sub>AlF<sub>6</sub> $\Rightarrow x_1d$  NaAlF<sub>4</sub>+2 $x_1d$  NaF (E)

it follows that the sum of the ions equals  $1 + 2d = k_{1/2}$ . Consequently d = 0.60.

Analogical calculations have been made also using the data presented by *Grjotheim et al.* [13]. The results are confronted in Table 3.

Drawing conclusions we may state that the application of the method of "the second component" to the study of the thermal dissociation of cryolite confirms the data obtained by other methods [2, 10], according to which it holds for cryolite that  $b \doteq 0.25$ .

## References

- Grjotheim, K., Contribution to the Theory of the Aluminium Electrolysis. Kgl. Norske Vidensk. Selsk. Skr., No. 5. F. Bruns, Trondheim, 1956.
- 2. Brynestad, J., Grjotheim, K., and Urnes, S., Met. Ital. 52, 495 (1960).
- 3. Frank, W. B. and Foster, L. M., J. Phys. Chem. 61, 1531 (1957).
- 4. Rolin, M., Bull. Soc. Chim. Fr. 1960, 677, 681.
- 5. Rolin, M. and Bernard, M., Bull. Soc. Chim. Fr. 1962, 429.
- 6. Paučírová, M., Matiašovský, K., and Malinovský, M., Rev. Roum. Chim. 15, 201 (1970).
- 7. Matiašovský, K., Paučírová, M., and Malinovský, M., Collect. Czech. Chem. Commun. 37, 1963 (1972).
- 8. Solomons, C., Clarke, J. H. R., and Bockris, J. O'M., J. Chem. Phys. 49, 445 (1968).
- 9. Dewing, E. W., Met. Trans. 3, 495, 2699 (1972).
- 10. Gilbert, B., Mamantov, G., and Begun, G. M., J. Chem. Phys. 62, 950 (1975).
- 11. Dewing, E. W. and Kouwe, E. Th., J. Electrochem. Soc. 122, 358 (1975).
- 12. Glasstone, S., Textbook of Physical Chemistry, 2nd Ed. Van Nostrand, New York; Mac Millan, London, 1947.
- 13. Grjotheim, K., Halvorsen, T., and Urnes, S., Can. J. Chem. 37, 1170 (1959).
- 14. Matiašovský, K. and Malinovský, M., Chem. Zvesti 19, 41 (1965).
- 15. Temkin, M., Acta Physicochim. URSS, 20, 411 (1945).
- 16. Petit, G. and Ngo Tuang, C. R. Acad. Sci. (Paris) C262, 243 (1966).
- 17. Koštenská, I. and Malinovský, M., Chem. Zvesti 28, 553 (1974).
- Kelley, K. K., Contributions to the Data on Theoretical Metallurgy, XIII. U.S. Bureau of Mines. Bulletin 584, Washington, 1960.
- 19. Malinovský, M. and Koštenská, I., Chem. Zvesti 28, 493 (1974).

Translated by M. Uhrová